

**Today, we will:**

- Discuss dimensional analysis of turbines
- Do an example problem – dimensional analysis with turbines
- Discuss piping networks – how to deal with pipes in series or in parallel

**b. Dimensionless parameters in turbine performance**

We perform exactly the same dimensional analysis for turbines as we did for pumps. Result:

Dimensionless Parameters:  $C_Q = \frac{\dot{V}}{\omega D^3}$  Capacity coefficient       $C_H = \frac{gH}{\omega^2 D^2}$  Head coefficient       $C_P = \frac{bhp}{\rho \omega^3 D^5}$  Power coefficient

$$\eta_{\text{turbine}} = \frac{bhp}{\rho \dot{V} g h} = \frac{C_P}{C_Q C_H}$$

$$\left[ \eta_{\text{pump}} = \frac{\rho \dot{V} g h}{bhp} = \frac{C_Q C_H}{C_P} \right]$$

there are not as important  
Re,  $\epsilon/D$

For turbines,  $C_P$  is used instead of  $C_Q$  as the independent parameter or  $\pi$

$$\begin{aligned} C_Q &= C_Q(C_P) \\ C_H &= C_H(C_P) \\ \eta_{\text{turbine}} &= \eta_{\text{turbine}}(C_P) \end{aligned}$$

[Power is more important in turbines than flow rate – flow rate is more important in pumps]

**Example: Scaling up a hydroturbine**

**Given:** An existing hydroturbine (A): Fluid is water at 20°C,  $D_A = 1.95$  m,  $\dot{n}_A = 120$  rpm,  $bhp_A = 220$  MW, and  $\dot{V}_A = 335$  m<sup>3</sup>/s at  $H_A = 72.4$  m. We are designing a new turbine (B) that is geometrically similar, still uses water at 20°C, and  $\dot{n}_B = 120$  rpm, but  $H_B = 97.4$  m. [Dam B has a higher gross head available than Dam A.]

**To do:** (a) Calculate  $D_B$  and  $\dot{V}_B$  for operation of turbine B at a homologous point.  
(b) Calculate  $bhp_B$  and estimate the turbine efficiency of both turbines.

**Solution:** dynamically similar

(a) At homologous points, the two turbines are dynamically similar. Apply the affinity laws:

$$C_{H,A} = \frac{gH_A}{\omega_A^2 D_A^2} = C_{H,B} = \frac{gH_B}{\omega_B^2 D_B^2} \rightarrow \text{solve for } D_B = D_A \left( \frac{\omega_A}{\omega_B} \right) \sqrt{\frac{H_B}{H_A}} = D_A \left( \frac{\dot{n}_A}{\dot{n}_B} \right) \sqrt{\frac{H_B}{H_A}}$$

Plug in numbers:  $D_B = (1.95 \text{ m}) \left( \frac{120 \text{ rpm}}{120 \text{ rpm}} \right) \sqrt{\frac{97.4 \text{ m}}{72.4 \text{ m}}} = 2.2618 \text{ m} \rightarrow D_B = 2.26 \text{ m}$

Similarly,  $C_{Q,A} = \frac{\dot{V}_A}{\omega_A D_A^3} = C_{Q,B} = \frac{\dot{V}_B}{\omega_B D_B^3} \rightarrow \dot{V}_B = \dot{V}_A \left( \frac{\omega_B}{\omega_A} \right) \left( \frac{D_B}{D_A} \right)^3 = \dot{V}_A \left( \frac{\dot{n}_B}{\dot{n}_A} \right) \left( \frac{D_B}{D_A} \right)^3$

Plug in numbers:  $\dot{V}_B = (335 \text{ m}^3/\text{s}) \left( \frac{120}{120} \right) \left( \frac{2.2618 \text{ m}}{1.95 \text{ m}} \right)^3 = 522.73 \text{ m}^3/\text{s} \rightarrow \dot{V}_B = 523 \text{ m}^3/\text{s}$

(b) Similarly,  $C_{P,A} = \frac{bhp_A}{\rho_A \omega_A^3 D_A^5} = C_{P,B} = \frac{bhp_B}{\rho_B \omega_B^3 D_B^5} \rightarrow \underline{bhp_B} = bhp_A \left( \frac{\rho_B}{\rho_A} \right) \left( \frac{\dot{n}_B}{\dot{n}_A} \right)^3 \left( \frac{D_B}{D_A} \right)^5$

Plug in numbers: *equate power coefficients*

$$bhp_B = (1)(1) \left( \frac{2.2618 \text{ m}}{1.95 \text{ m}} \right)^5 = 461.82 \text{ MW}$$

$$= 462 \text{ MW}$$

Finally, the efficiency is calculated for each turbine:

$$\eta_{\text{turbine},A} = \frac{bhp_A}{\rho_A g H_A \dot{V}_A} = \frac{220,000,000 \text{ W}}{\left( 1000 \frac{\text{kg}}{\text{m}^3} \right) \left( 9.81 \frac{\text{m}}{\text{s}^2} \right) 72.4 \text{ m} \left( 335 \frac{\text{m}^3}{\text{s}} \right)} \left( \frac{\text{N} \cdot \text{m}}{\text{W} \cdot \text{s}} \right) \left( \frac{\text{kg} \cdot \text{m}}{\text{s}^2 \cdot \text{N}} \right) = 92.5\%$$

$$\eta_{\text{turbine},B} = \frac{bhp_B}{\rho_B g H_B \dot{V}_B} = \frac{461,820,979 \text{ W}}{\left( 1000 \frac{\text{kg}}{\text{m}^3} \right) \left( 9.81 \frac{\text{m}}{\text{s}^2} \right) 97.4 \text{ m} \left( 522.728 \frac{\text{m}^3}{\text{s}} \right)} \left( \frac{\text{N} \cdot \text{m}}{\text{W} \cdot \text{s}} \right) \left( \frac{\text{kg} \cdot \text{m}}{\text{s}^2 \cdot \text{N}} \right) = 92.5\%$$

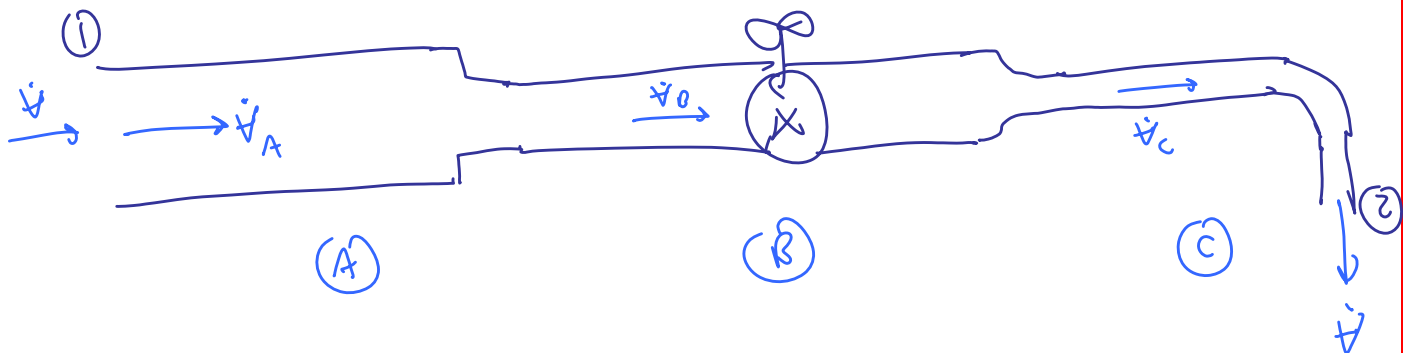
$\eta$ 's are = 1

they must be.

## F. Piping Networks

1. Pipes in Series — We already know how to do this

$$\dot{V} = \dot{V}_A = \dot{V}_B = \dot{V}_C$$



$$V_A \neq V_B \neq V_C \quad \text{since} \quad D_A \neq D_B \neq D_C$$

$$\therefore Re_A \neq Re_B \neq Re_C, \quad \left( \frac{\epsilon}{D} \right)_A \neq \left( \frac{\epsilon}{D} \right)_B \neq \left( \frac{\epsilon}{D} \right)_C$$

$$\rightarrow f_A \neq f_B \neq f_C$$

But we can apply 1 energy eq from (1) to (2):

$$\frac{P_1}{\rho g} + \alpha_1 \frac{V_1^2}{2g} + \dots$$

$$+ h_L$$

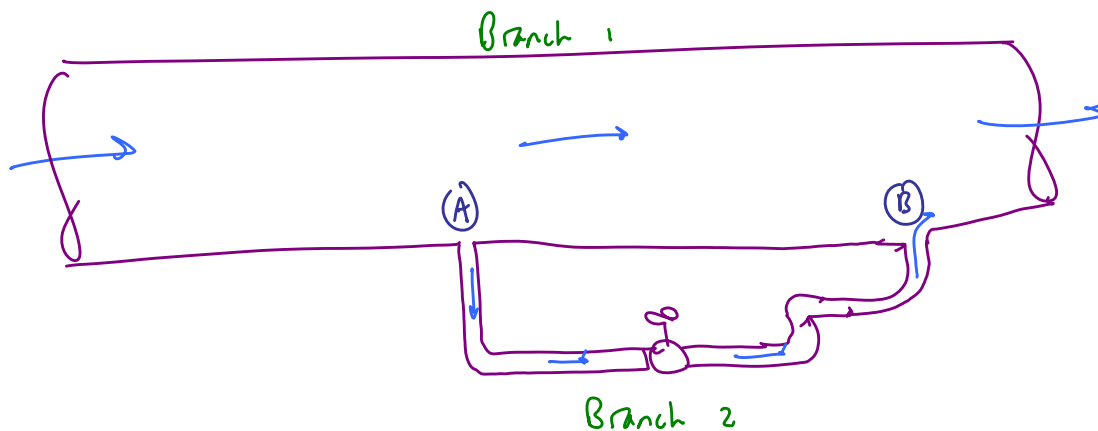
$$=$$

$$h_L = \sum_i f_i \frac{L_i}{D_i} \frac{V_i^2}{2g} + \sum_j K_{L,j} \frac{V_j^2}{2g}$$

$\uparrow$  sum over all sections of piping       $\uparrow$  sum over all minor losses

2. Pipes in Parallel - more difficult since  $\dot{V}$  not the same in each branch

eg.



Which branch has the larger head loss from A to B?

(A) Branch 1

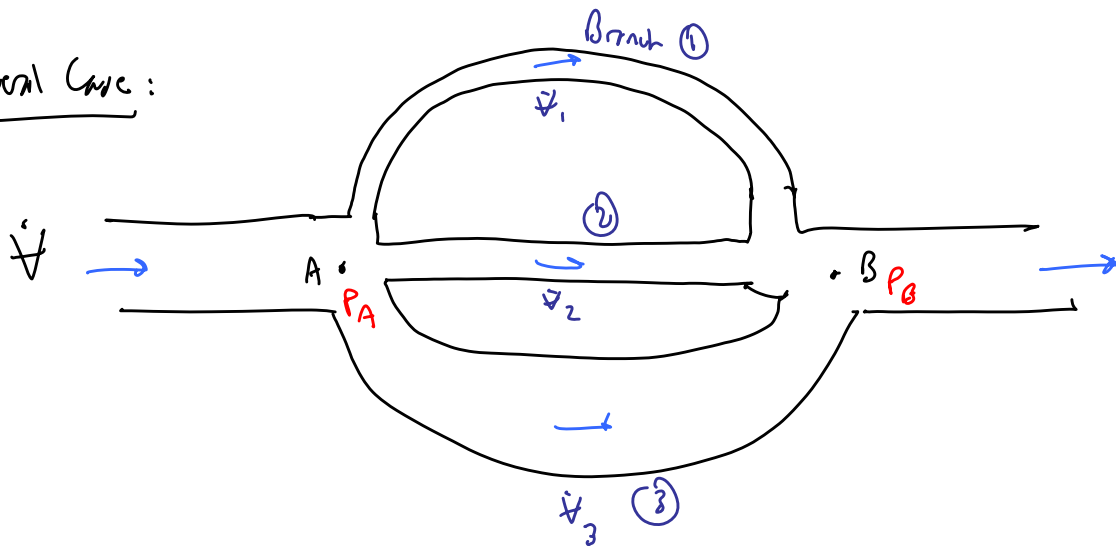
(B) Branch 2

(C) Neither (head loss is the same through either branch)

$$h_L = \frac{P_A - P_B}{\rho g}$$

$\dot{V}$  will adjust itself such that  $\Delta P$  is the same through both branches,  $\rightarrow \dot{V}_{\text{Branch 2}} \ll \dot{V}_{\text{Branch 1}}$

General Case:

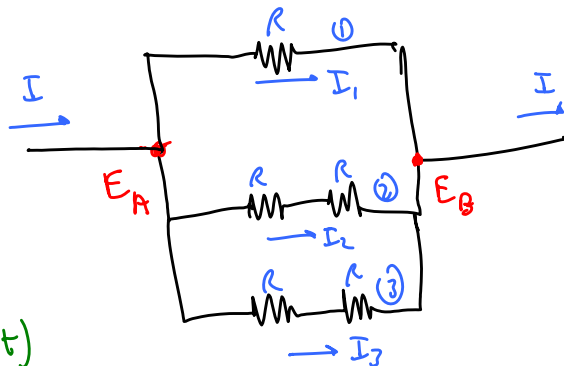


$$\dot{V} = \dot{V}_1 + \dot{V}_2 + \dot{V}_3 + \dots$$

But since  $P_A - P_B$  is the same, same head loss through any section

$\dot{V}$ 's will automatically adjust to the "correct"  $\dot{V}$  such that these eqs are met

ELECTRICAL ANALOGY:



major: minor losses

$\dot{V} \Leftrightarrow I$  (current)  
is analogous to

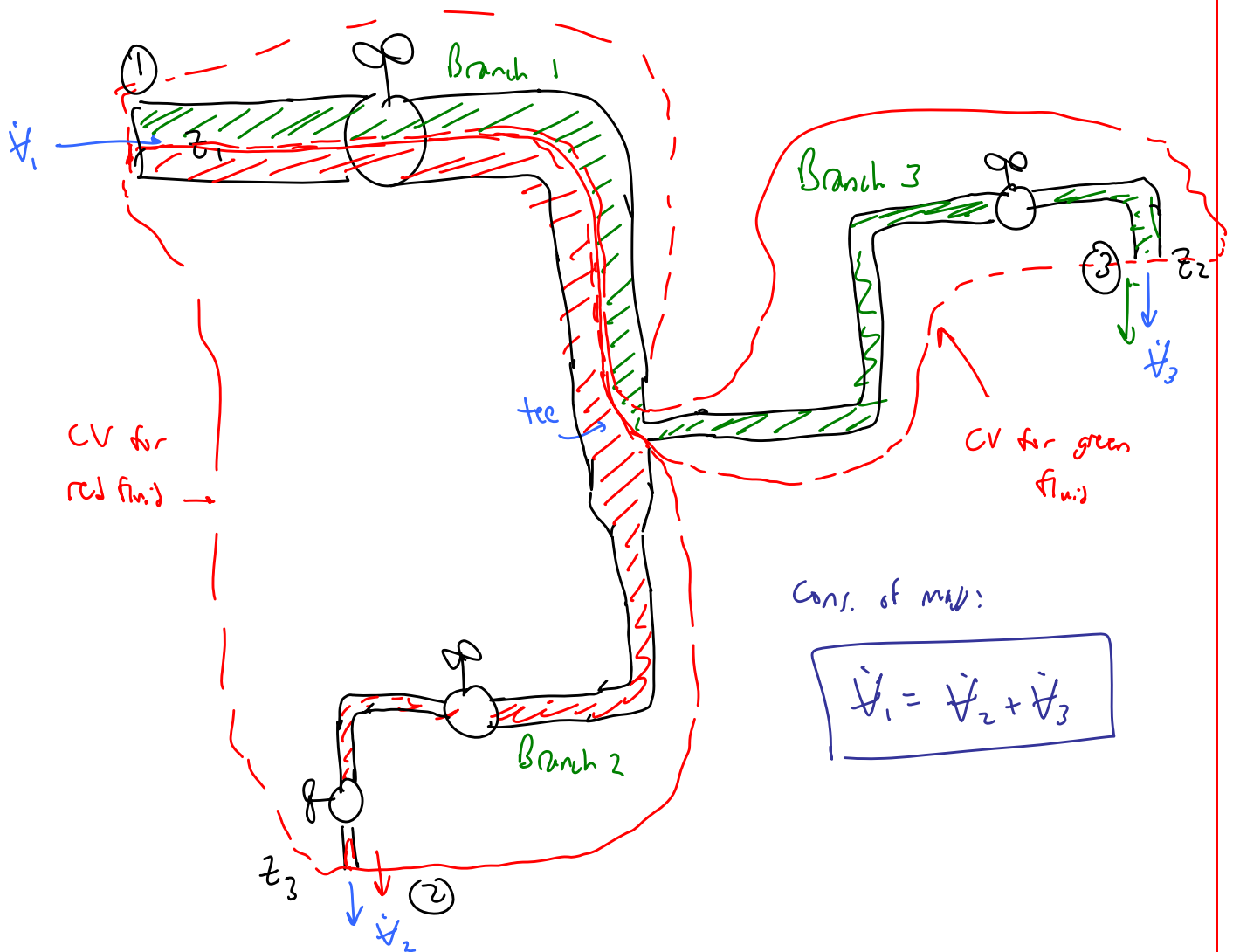
$P \Leftrightarrow E$  (Voltage)

Components of  $h_L \Leftrightarrow R$  (resistance)

$E_A - E_B =$  the same regardless of the branch: the currents will adjust appropriately

### 3. Complex Piping network

Qualitative eg.



Cons of energy in head form  $\rightarrow$  Apply to the water flowing through Branch 1 & 2 separately from 1 & 3

from ① to ②:

$$\frac{P_1}{\rho g} + \alpha_1 \frac{V_1^2}{2g} + z_1 + \cancel{h_{\text{pump},1-2}} = \frac{P_2}{\rho g} + \alpha_2 \frac{V_2^2}{2g} + z_2 + \cancel{h_{\text{friction},1-2}} + h_{L,1-2}$$

from ① to ③:

$$\frac{P_1}{\rho g} + \alpha_1 \frac{V_1^2}{2g} + z_1 + \cancel{h_{\text{pump},1-3}} = \frac{P_3}{\rho g} + \alpha_3 \frac{V_3^2}{2g} + z_3 + \cancel{h_{\text{friction},1-3}} + h_{L,1-3}$$

Notes: •  $h_{L, 1 \rightarrow 2}$  includes heat losses through Branches 1 & 2

•  $h_{L, 1 \rightarrow 3}$  " " " " " 1 & 3

• Must use appropriate  $V$ 's ( $V_1$ ,  $V_2$ , or  $V_3$ ) to calculate  $Re$  through each branch

• Each branch has a different  $V$ ,  $Re$ ,  $\epsilon/D$ ,  $f$  (Moody chart),  $\sum K_L$  etc.

• Think of the red fluid as two pipes in series, Branches  
① & ②

• Think of the green fluid as " " " " "  
① & ③

To solve - must solve a set of many simultaneous eq's

$$Re_1 = \frac{\rho V_1 D_1}{\mu} \quad Re_2 = \frac{\rho V_2 D_2}{\mu} \quad Re_3 = \frac{\rho V_3 D_3}{\mu}$$

$$f_1 = \text{moody chart}(Re_1, \epsilon_1/D_1) \quad f_2 = \text{moody chart}(Re_2, \epsilon_2/D_2)$$

$$f_3 = \text{moody chart}(Re_3, \epsilon_3/D_3)$$

There will be  $\sum K_{L,1}$ ,  $\sum K_{L,2}$ ,  $\sum K_{L,3}$  &  $h_{L,1}$ ,  $h_{L,2}$ ,  $h_{L,3}$

$$\dot{V}_1 = \frac{\pi D_1^2}{4} V_1$$

$$\dot{V}_2 = \frac{\pi D_2^2}{4} V_2$$

$$\dot{V}_3 = \frac{\pi D_3^2}{4} V_3$$

$$\dot{V}_1 = \dot{V}_2 + \dot{V}_3$$

★ MUST SOLVE ALL OF THESE EQUATIONS SIMULTANEOUSLY (I use EES)