

Today, we will:

- Discuss **Terminal Settling Speed** in quiescent air due to gravity, also called **Gravimetric Settling**
- Discuss an **Approximation** for terminal settling speed for the case of **Stokes Flow**
- Do an example problem

Review of Air Properties and Equations of Particle Motion:

Air property equations: $\rho = \frac{P}{R_{\text{air}} T}$, where $R_{\text{air}} = 0.2870 \frac{\text{kJ}}{\text{kg} \cdot \text{K}} = 287.0 \frac{\text{J}}{\text{kg} \cdot \text{K}} = 287.0 \frac{\text{m}^2}{\text{s}^2 \cdot \text{K}}$

and viscosity comes from the **Sutherland Equation** $\mu \approx \mu_s \left(\frac{T}{T_{s,0}} \right)^{3/2} \frac{T_{s,0} + T_s}{T + T_s}$,

where $T_{s,0} = 298.15 \text{ K}$, $T_s = 110.4 \text{ K}$, $\mu_s = 1.849 \times 10^{-5} \frac{\text{kg}}{\text{m} \cdot \text{s}}$.

Relative particle velocity = $\vec{v}_r = \vec{v} - \vec{U}$, where \vec{v} = particle velocity and \vec{U} = air velocity.

Drag force on a spherical particle = $\vec{F}_{\text{drag}} = -\frac{1}{8} \rho \frac{C_D}{C} \pi D_p^2 \vec{v}_r |\vec{v}_r|$, where C_D comes from the

Morrison Eq. $C_D \approx \frac{24}{\text{Re}} + \frac{2.6 \left(\frac{\text{Re}}{5.0} \right)}{1 + \left(\frac{\text{Re}}{5.0} \right)^{1.52}} + \frac{0.411 \left(\frac{\text{Re}}{2.63 \times 10^5} \right)^{-7.94}}{1 + \left(\frac{\text{Re}}{2.63 \times 10^5} \right)^{-8.00}} + \frac{0.25 \left(\frac{\text{Re}}{10^6} \right)}{1 + \left(\frac{\text{Re}}{10^6} \right)}$ for $\text{Re} < 10^6$,

C is the **Cunningham Correction Factor** $C = 1 + \text{Kn} \left[2.514 + 0.80 \exp \left(-\frac{0.55}{\text{Kn}} \right) \right]$, Kn is the

Knudsen number $\text{Kn} = \frac{\lambda}{D_p}$, λ is the **mean free path** of the air $\lambda = \frac{\mu}{0.499 \sqrt{8\rho P}}$, and Re is

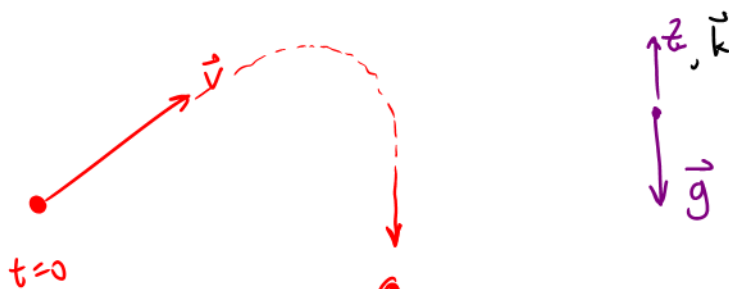
the **Reynolds number** relative to the moving particle $\text{Re} = \frac{\rho |\vec{v}_r| D_p}{\mu}$.

Equation of motion for a spherical particle: $m_p \vec{a}_p = \vec{F}_{\text{grav}} + \vec{F}_{\text{drag}}$

$$m_p \frac{d\vec{v}}{dt} = \frac{\pi D_p^3}{6} (\rho_p - \rho) \vec{g} - \frac{1}{8} \rho \frac{C_D}{C} \pi D_p^2 \vec{v}_r |\vec{v}_r|$$

The above equations are valid for the standard **continuum fluid approximation** (fluid is treated as a continuum, not worried about free molecular effects). But, for very small particles in air, the fluid is no longer a continuum, and **free molecular effects** are important. We have taken this into account by the Cunningham Correction Factor.

Simplest Application – Terminal Settling Speed in Quiescent Air:



★ $V_t =$ Terminal Settling Speed

$V_t = \text{const}$

Here $\vec{U} = 0$



$$\vec{V} = -V_t \vec{k}$$

@ steady settling speed $\rightarrow \frac{d\vec{V}}{dt} = 0$

$$\left[\frac{d\vec{V}}{dt} \right] = -V_t^2 \vec{k}$$

$$0 = -(\rho_p - \rho)g + \frac{3}{4} \rho \frac{C_D}{C} \frac{1}{D_p} V_t^2$$

Terminal settling speed:

$$V_t = \sqrt{\frac{4(\rho_p - \rho)gD_p}{3\rho} \frac{C}{C_D}}$$

but $C_D = C_D(Re)$, where

$$Re = \frac{\rho V_t D_p}{\mu}$$

★ GENERAL CASE

$C_D = C_D(Re)$, $Re = f(V_t)$

★ IMPLICIT EQ



★ MUST ITERATE

Simplest Case of Terminal Settling Speed in Quiescent Air – Stokes Flow Approximation:

THIS IS AN APPROXIMATION!

★ STOKES FLOW → $Re \lesssim 0.1$ ∴ then

$$C_D = \frac{24}{Re} = \frac{24 \mu}{\rho V_t D_p}$$

• Plug this C_D into our general eq for V_t

$$V_t^2 = \frac{4}{3} \frac{(\rho_p - \rho) g D_p}{\rho} \frac{C_D V_t D_p}{24 \mu}$$

$$V_t = \frac{4}{3(24)} (\rho_p - \rho) g D_p^2 \frac{C}{\mu}$$

$$V_t = \frac{\rho_p - \rho}{18} g D_p^2 \frac{C}{\mu}$$

Terminal Settling Speed
for Stokes Flow Approx.

VALID ONLY IF $Re \lesssim 0.1$

Example: Stokes Flow Settling Speed

Given: A spherical particle falls in quiescent air. Here are some properties:

- $P = 101.325 \text{ kPa}$
 - $T = 25^\circ\text{C} = 298.15 \text{ K}$
 - $D_p = 10.0 \mu\text{m}$
 - $\rho_p = 1000 \text{ kg/m}^3$ (unit density)
- } SATP

To do: Calculate the Stokes flow terminal settling speed V_t . Repeat for $D_p = 100 \mu\text{m}$.

Solution:

First we need the air properties at this temperature and pressure:

At SATP → we prop. from Eq 5.1.

$$\rho = 1.184 \frac{\text{kg}}{\text{m}^3} \quad \mu = 1.849 \times 10^{-5} \frac{\text{kg}}{\text{m}\cdot\text{s}} \quad \lambda = 0.06704 \mu\text{m}$$

Next we need to calculate the CCF (Cunningham Correction Factor) C :

$$C = 1 + \text{Kn} \left[2.514 + 0.80 \exp\left(-\frac{0.55}{\text{Kn}}\right) \right], \text{ where } \text{Kn} = \frac{\lambda}{D_p} \rightarrow \frac{0.06704 \mu\text{m}}{10.0 \mu\text{m}} = 0.006704$$

$$\underline{C = 1.0169}$$

Finally, we apply the Stokes flow terminal settling speed approximate equation:

$$V_t = \frac{\rho_p - \rho}{18} D_p^2 g \frac{C}{\mu}$$

$$V_t = \frac{(1000 - 1.184) \frac{\text{kg}}{\text{m}^3}}{18} \frac{(10.0 \times 10^{-6} \text{ m})^2 (9.807 \frac{\text{m}}{\text{s}^2})(1.0169)}{1.849 \times 10^{-5} \frac{\text{kg}}{\text{m} \cdot \text{s}}}$$

$$V_t = 0.00299 \frac{\text{m}}{\text{s}}$$

Notice how small!

e.g. in one minute

$$\Delta z = V_t \cdot \Delta t = (0.00299 \frac{\text{m}}{\text{s}})(1 \text{ min}) \left(\frac{60 \text{ s}}{\text{min}} \right)$$

$$\Delta z = 0.1796 \text{ m} = \underline{18 \text{ cm}}$$

CHECK

$$\star Re = \frac{\rho V_t D_p}{\mu} = \frac{(1.184 \frac{\text{kg}}{\text{m}^3})(0.002993 \frac{\text{m}}{\text{s}})(10.0 \times 10^{-6} \text{ m})}{1.849 \times 10^{-5} \frac{\text{kg}}{\text{m} \cdot \text{s}}} = 0.00192$$

\star STOKES FLOW APPROX. IS VALID HERE $< \underline{0.1}$

• REPEAT @ $D_p = 100 \mu\text{m}$

~~$$V_t = 0.295 \frac{\text{m}}{\text{s}}$$~~

→ STOKES NOT VALID FOR THIS CASE \star

~~check $Re = 1.89 \approx 0.1$~~

WHAT TO DO? Go back to our General Eq

$$V_t = \sqrt{\frac{4}{3} \frac{\rho_p - \rho}{\rho} g D_p \frac{C}{C_0}}$$

\star MUST ITERATE