

**Today, we will:**

- Do some review example problems, partial pressure, mol fraction, flow rates, etc.
- Discuss species mass flow rates, and various definitions of pollutant concentration

**Example: Partial pressure****Given:**

- The mol fraction of CO (carbon monoxide) in a container is 56.0 PPM. <sup>with air</sup>
- The molecular weight of CO is 28.0 kg/kmol.
- The temperature is 20°C and the pressure is 99.5 kPa in the container.

**To do:** Calculate the partial pressure of CO in the container.

**Solution:**

(a)  $y_j = \frac{P_j}{P}$  here let  $j = \text{CO}$   $y_j = 56.0 \text{ PPM}$   
 $P_j = y_j \cdot P$   $y_j = 56.0 \times 10^{-6}$   
 $P_j = (56.0 \times 10^{-6})(99.5 \text{ kPa}) = 5.572 \times 10^{-3} \text{ kPa}$   
 ✱ Small! →  $P_j = 5.57 \times 10^{-3} \text{ kPa}$

(b) if  $V = 1.20 \text{ m}^3$ , calculate  $V_j$   
 Soln.  $y_j = \frac{V_j}{V} \rightarrow V_j = y_j V = (56.0 \times 10^{-6})(1.20 \text{ m}^3) = 0.000672 \text{ m}^3$   
 $\times \left(\frac{100 \text{ cm}}{\text{m}}\right)^3 = \underline{\underline{67.2 \text{ cm}^3}}$

(c) Calc. the mass of the CO in grams  $T = 20 + 273.15 = 293.15 \text{ K}$

Soln: Use Ideal gas law:

$$P_j V = n_j R_u T$$

$$n_j = \frac{m_j}{M_j}$$

$$M_j = 28.0 \frac{\text{kg}}{\text{kmol}}$$

$$m_j = \frac{P_j V M_j}{R_u T}$$

$$m_j = \frac{(5.572 \times 10^{-3} \text{ kPa})(1.20 \text{ m}^3)(28.0 \text{ kg/kmol})}{(8.314 \frac{\text{kJ}}{\text{kmol} \cdot \text{K}})(293.15 \text{ K})} \left( \frac{1000 \text{ g}}{\text{kg}} \right) \left( \frac{\text{kJ}}{\text{kN} \cdot \text{m}} \right) \left( \frac{\text{kN}}{\text{m}^2 \cdot \text{kPa}} \right) = \underline{\underline{0.0768 \text{ g}}}$$

## Concentrations of air pollutants

• Mass concentration  $C_j = \frac{\text{mass of species } j}{V \text{ of mixture}} = \boxed{C_j = \frac{m_j}{V}}$

dim:  $\{C_j\} = \left\{ \frac{m}{L^3} \right\}$     unit  $\rightarrow \frac{mg}{m^3}, \frac{mg}{L}, \text{ etc.}$

• molar concentration

$$C_{\text{molar},j} = \frac{\# \text{ mols of species } j}{V \text{ of mixture}} = \frac{n_j}{V}$$

dim  $\{C_{\text{molar},j}\} = \left\{ \frac{N}{L^3} \right\}$     unit  $\frac{\text{mol}}{m^3}, \frac{\text{mol}}{ft^3}, \frac{\text{mol}}{L}, \text{ etc.}$

Conversion: Since  $m_j = n_j M_j \rightarrow C_{\text{molar},j} = \frac{n_j}{V} \frac{M_j}{M_j} = \frac{1}{M_j} \frac{m_j}{V} = \frac{C_j}{M_j}$

$$\boxed{C_{\text{molar},j} = \frac{C_j}{M_j}}$$

More conversion: For ideal gas mixture

$C_j = \frac{m_j}{V} = \text{mass conc.}$

$(m_j = n_j M_j)$

but  $P_j V = n_j R_u T = \frac{m_j}{M_j} R_u T$

$V = \frac{m_j}{M_j} \frac{R_u T}{P_j}$

$C_j = \frac{\cancel{m_j} M_j P_j}{\cancel{m_j} R_u T P} \rightarrow y_j$

$C_j = y_j \frac{M_j}{R_u} \frac{P}{T}$

(1)

- Mol fraction  $y_j$  is independent of  $P$  &  $T$
  - Mass concentration  $C_j$  is dependent on  $P$  &  $T$
  - molar "  $C_{molar,j}$  is dependent on  $P$  &  $T$
- ★

Mass flow rate of species  $j$

$\dot{m} = \rho Q$  = total or bulk mass flow rate of the mixture

Define  $\dot{m}_j$  = mass flow rate of species  $j$

$$\dot{m}_j = \frac{\text{mass of } j}{\text{time}} = \frac{\text{mass of } j}{\text{vol.}} \cdot \frac{\text{vol.}}{\text{time}} = C_j \cdot Q$$

$\dot{m}_j = C_j Q$

Caution: This  $Q$  is actual  $Q$  not the standard  $Q$

### Example: Volume and mass flow rate

#### Given:

- The bulk volume flow rate of an air/ammonia mixture is 1000 ACFM through a duct. → actual ft<sup>3</sup>/min
- The air contains 5.0 PPM of ammonia vapor ( $M_{\text{ammonia}} = 17.0 \text{ g/mol}$ ).
- The temperature is 200.°C (473.15 K) and the pressure is 90. kPa.

(a) To do: Calculate the bulk volume flow rate in SCFM.

**Solution:**  $Q_{\text{STP}} = Q_{\text{actual}} \frac{P}{P_{\text{STP}}} \frac{T_{\text{STP}}}{T} = \left(1000 \frac{\text{ft}^3}{\text{min}}\right) \left(\frac{90. \text{kPa}}{101.325 \text{kPa}}\right) \left(\frac{298.15 \text{ K}}{473.15 \text{ K}}\right) = 559.7 \approx \underline{\underline{560 \text{ SCFM}}}$

(b) To do: Calculate the ammonia mass concentration.

**Solution:**  $C_j = y_j \frac{P}{T} \frac{M_j}{R_u} = \left(5.0 \times 10^{-6} \frac{\text{kmol, am}}{\text{kmol}}\right) \left(\frac{90.0 \text{ kPa}}{473.15 \text{ K}}\right) \frac{17.0 \frac{\text{kg, am}}{\text{kmol, am}}}{8.314 \frac{\text{kJ}}{\text{kmol} \cdot \text{K}}} \left(\frac{\text{kJ}}{\text{kN} \cdot \text{m}}\right) \left(\frac{\text{kN}}{\text{m}^2 \cdot \text{kPa}}\right) \left(\frac{10^6 \text{ mg, am}}{\text{kg, am}}\right)$

$C_j = 1.9447 \frac{\text{mg}}{\text{m}^3} \rightarrow \underline{\underline{C_j = 1.9 \frac{\text{mg}}{\text{m}^3}}}$

(c) To do: Calculate the emission rate  $\dot{m}_j$  of ammonia into the atmosphere in g/hr.

#### Solution:

$$\dot{m}_j = C_j Q_{\text{actual}}$$

$$\dot{m}_j = \left(1.9447 \frac{\text{mg}}{\text{m}^3}\right) \left(1000 \frac{\text{ft}^3}{\text{min}}\right) \left(\frac{0.3048 \text{ m}}{\text{ft}}\right)^3 \left(\frac{60 \text{ min}}{\text{hr}}\right) \left(\frac{1 \text{ g}}{1000 \text{ mg}}\right) = 3.30406 \frac{\text{g}}{\text{hr}}$$

$$\underline{\underline{\dot{m}_j = 3.3 \frac{\text{g}}{\text{hr}}}}$$