

In this lesson, we will:

- Derive the **Reynolds Transport Theorem (RTT)** by application of **Leibniz Theorem**
- Discuss **material volumes** and how the RTT is a **link** between **Lagrangian** and **Eulerian** descriptions

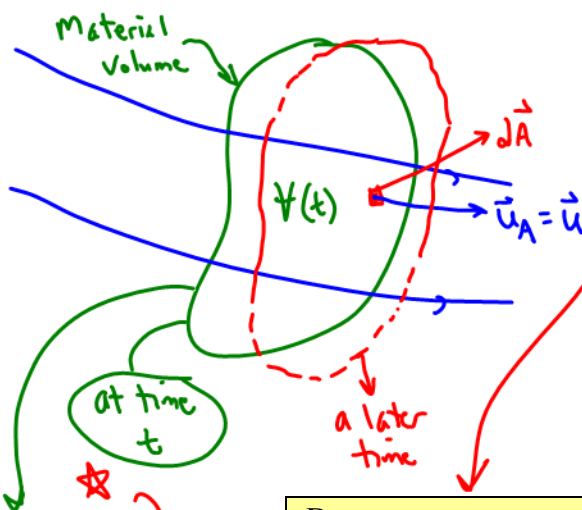
### Derivation of the Reynolds Transport Theorem

Start with the **3-D Leibniz Theorem** for function or property  $\phi$ , a function of  $\vec{x}$  and  $t$ ,

$\forall(t)$  moves  
Independently of  
the fluid

$$\frac{d}{dt} \int_{V(t)} \phi(\vec{x}, t) dV = \int_{V(t)} \frac{\partial \phi(\vec{x}, t)}{\partial t} dV + \oint_{A(t)} \phi(\vec{x}, t) \vec{u}_A \cdot d\vec{A}$$

For the **special case** of a **material volume** (a volume that moves with the fluid),  $\vec{u}_A = \vec{u}$



THIS MATERIAL VOLUME  
IS A SYSTEM [closed system]

ALWAYS CONTAINS THE SAME MASS

SINCE  $\forall(t)$  IS A MATERIAL VOLUME, WE USE

$\frac{D}{Dt}$  instead of  $\frac{d}{dt}$

**CONTROL VOLUME**

$$\frac{D}{Dt} \int_{V(t)} \phi(\vec{x}, t) dV = \int_{V(t)} \frac{\partial \phi(\vec{x}, t)}{\partial t} dV + \oint_{A(t)} \phi(\vec{x}, t) \vec{u} \cdot d\vec{A}$$

(1)

But, **at this instant in time**, since the **control volume is the material volume** (they are **coincident**), we can set the volume as the control volume and the area as the control surface,

$CV(t)$

$CS(t)$

$$\frac{D}{Dt} \int_{V(t)} \phi(\vec{x}, t) dV = \int_{CV(t)} \frac{\partial \phi(\vec{x}, t)}{\partial t} dV + \oint_{CS(t)} \phi(\vec{x}, t) \vec{u} \cdot d\vec{A}$$

★ THIS IS THE  
**R.T.T.!**

(2)

LHS is the  
material volume

RHS is the  
control volume

★ VALID AT ANY INSTANT IN TIME

$\vec{u}_A = \vec{u}$

WE CHOOSE  $\forall(t)$   
TO BE THE CV  
@ time  $t$   
(material volume)

$\forall(t) \equiv CV(t)$   
are coincident  
@ time  $t$

SUMMARY:  $\forall(t) = CV(t)$

$A(t) = \underline{CS(t)}$

## Summary of the Reynolds Transport Theorem

We applied Leibniz Theorem to the *special case* in which  $V(t)$  is a **material volume** – a **volume that moves with the fluid**. As the fluid moves and distorts in the flow field, the material volume moves and distorts with it since, by definition, the material volume always contains the same physical mass of fluid. It follows that area  $A$  also moves with the local fluid velocity. Thus,  $\vec{u}_A = \vec{u}$  where  $\vec{u}$  is the fluid velocity, a function of space and time in the Eulerian description. To stress that  $V(t)$  is a **material volume**,  $D/Dt$  is used instead of  $d/dt$  for time derivatives following material volumes.

The **Reynolds Transport Theorem (RTT)** for a **moving control volume** is thus

$$\frac{D}{Dt} \int_{V(t)} \phi(\vec{x}, t) dV = \int_{CV(t)} \frac{\partial \phi(\vec{x}, t)}{\partial t} dV + \oint_{CS(t)} \phi(\vec{x}, t) \vec{u} \cdot d\vec{A}, \text{ where } \vec{u} \text{ is the absolute velocity of}$$

**the fluid**,  $CV(t)$  is the **control volume**, and  $CS(t)$  is the **control surface**. In this general form of the Reynolds Transport Theorem, **the control volume can be moving and distorting in any arbitrary fashion**.

This is equivalent to 
$$\frac{D}{Dt} \int_{V(t)} \phi(\vec{x}, t) dV = \frac{d}{dt} \int_{CV(t)} \phi(\vec{x}, t) dV + \oint_{CS(t)} \phi(\vec{x}, t) \vec{u}_{\text{relative}} \cdot d\vec{A}, \text{ where}$$

$\vec{u}_{\text{relative}} = \vec{u} - \vec{u}_{CS}$  is **relative velocity**, the fluid velocity **relative to the control surface**.

A simplification of the general Reynolds Transport Theorem is possible if the control volume is fixed in space. In such a case, the relative velocity of the fluid is identical to its absolute velocity. So, the **Reynolds Transport Theorem for a fixed control volume** is

$$\frac{D}{Dt} \int_{V(t)} \phi(\vec{x}, t) dV = \int_{CV} \frac{\partial \phi(\vec{x}, t)}{\partial t} dV + \oint_{CS} \phi(\vec{x}, t) \vec{u} \cdot d\vec{A}. \text{ Or, since the order of integration or}$$

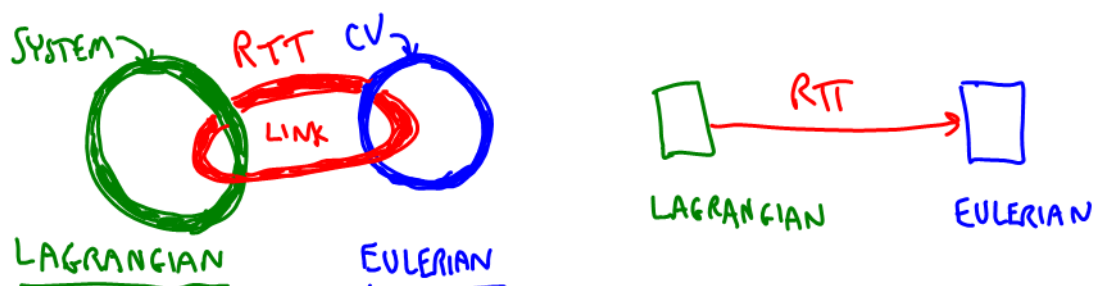
differentiation does not matter, 
$$\frac{D}{Dt} \int_{V(t)} \phi(\vec{x}, t) dV = \frac{d}{dt} \int_{CV} \phi(\vec{x}, t) dV + \oint_{CS} \phi(\vec{x}, t) \vec{u} \cdot d\vec{A}.$$

## Usefulness of the Reynolds Transport Theorem

The Reynolds Transport Theorem, in any of its forms above, contains a material volume on the left-hand side (LHS) and control volumes and control surfaces on the right-hand side (RHS). Thus, the **LHS is in the Lagrangian or system frame of reference**, while the **RHS is in the Eulerian or control volume frame of reference**.

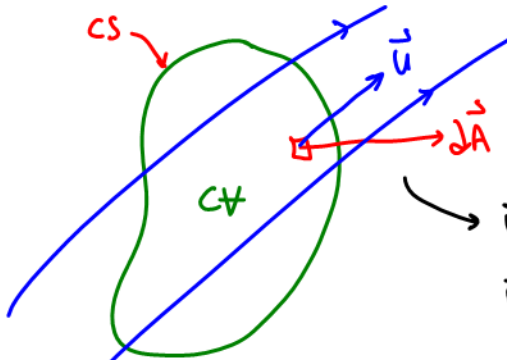
**The usefulness of the Reynolds Transport Theorem is that it bridges the gap between the Lagrangian and Eulerian descriptions or frames of reference.** ★

It thus enables us to transform conservation laws (which apply directly to Lagrangian material volumes) into Eulerian forms, which are usually more desirable in fluid mechanics.



## The Right-Most Term in the Reynolds Transport Theorem

$$\frac{D}{Dt} \int_{V(t)} \phi(\vec{x}, t) dV = \int_{CV(t)} \frac{\partial \phi(\vec{x}, t)}{\partial t} dV + \oint_{CS(t)} \phi(\vec{x}, t) \vec{u} \cdot d\vec{A}$$



$\vec{u} \cdot d\vec{A}$  is the volume flow rate of fluid crossing area element  $dA$

$\vec{u} \cdot d\vec{A}$  is  $\oplus$  if  $\vec{u}$  is "out"  
 $\vec{u} \cdot d\vec{A}$  is  $\ominus$  if  $\vec{u}$  is "in"

$\phi$  is typically a quantity per unit volume

WE LET  $\Phi = \phi \cdot \text{volume}$

$$\oint_{CS} \phi \vec{u} \cdot d\vec{A} = \text{NET RATE OF } (\phi \cdot \text{volume}) \text{ FLOW } \underline{\underline{\text{OUT}}} \text{ OF THE CS}$$

E.G., Let  $\phi = \rho = \frac{\text{mass}}{\text{Volume}} \rightarrow \Phi = \phi \cdot \text{volume} = \text{mass}$

$$\oint_{CS} \rho \vec{u} \cdot d\vec{A} = \underline{\underline{\text{NET RATE OF MASS FLOW OUT OF THE CS}}}$$

Dimensions

$$\left\{ \frac{m}{L^3} \frac{L}{t} L^2 \right\} = \left\{ \frac{m}{t} \right\} \checkmark$$

## Terms in the Reynolds Transport Theorem

$$\frac{D}{Dt} \int_{V(t)} \phi(\vec{x}, t) dV = \int_{CV(t)} \frac{\partial \phi(\vec{x}, t)}{\partial t} dV + \oint_{CS(t)} \phi(\vec{x}, t) \vec{u} \cdot d\vec{A}$$

TOTAL RATE OF  
CHANGE OF  $\Phi$   
FOLLOWING A  
MATERIAL VOLUME  
SYSTEM

LAGRANGIAN

RATE OF CHANGE  
OF  $\Phi$  DUE TO  
UNSTEADINESS OF  $\phi$   
WITHIN THE CV

RATE OF CHANGE  
OF  $\Phi$  DUE TO  
NET OUTFLOW  
OF  $\Phi$  THROUGH  
THE CS

CONTROL VOLUME

EULERIAN

CONSERVATION LAWS  
(FUNDAMENTALLY IN  
LAGRANGIAN FRAME)

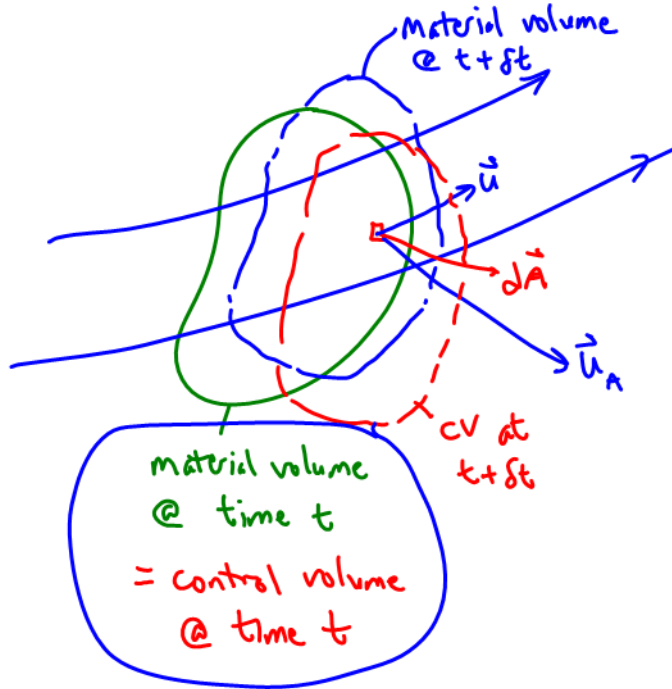
RTT →

EULERIAN

## Moving and/or Deforming Control Volume

$$\frac{D}{Dt} \int_{V(t)} \phi(\vec{x}, t) dV = \int_{CV(t)} \frac{\partial \phi(\vec{x}, t)}{\partial t} dV + \oint_{CS(t)} \phi(\vec{x}, t) \vec{u} \cdot d\vec{A} \quad \star$$

★ GENERAL CASE → CV moves independently of the material volume  
 .. .. flow



Recall, 3-D Leibniz holds at any instant in time  
 ∴ RTT holds at any instant in time

$$\vec{u} \Rightarrow u_i$$

$$\vec{x} \Rightarrow x_i \text{ or } x_j \text{ or } x_k$$

## Reynolds Transport Theorem in Tensor Notation

Start with the RTT in vector notation for property  $\phi$ , a function of  $\vec{x}$  and  $t$ ,

$$\frac{D}{Dt} \int_{V(t)} \phi(\vec{x}, t) dV = \int_{CV(t)} \frac{\partial \phi(\vec{x}, t)}{\partial t} dV + \oint_{CS(t)} \phi(\vec{x}, t) \vec{u} \cdot d\vec{A}$$

In tensor notation  $\phi = \phi(x_j, t)$ , and the RTT becomes

$$\frac{D}{Dt} \int_{V(t)} \phi(x_j, t) dV = \int_{CV(t)} \frac{\partial \phi(x_j, t)}{\partial t} dV + \oint_{CS(t)} \phi(x_j, t) u_i dA_i$$