

Today, we will:

- Finish modeling the tke equation (the additional transport eq. for one-equation turbulence models)
- Discuss closure for two-equation turbulence models, specifically the $k-\epsilon$ model.
- If time, begin to discuss how to treat the near-wall region.

Recall, the high-Reynolds # form of the tke. eq

Exact:
$$\frac{DK}{Dt} = \underbrace{\frac{\partial}{\partial x_j} (\text{~~~~~})}_{\substack{\text{Transport or} \\ \text{Diffusion}}} - \underbrace{\overline{u_i u_j} \frac{\partial U_i}{\partial x_j}}_{\substack{\text{Production}}} - \underbrace{\epsilon}_{\substack{\text{Dissipation}}}$$

Total rate of change
Transport or Diffusion
Production
Dissipation

↓
↓
↓
?

Leave as is
Gradient Diffusion model
Express in terms of ν_e

Modeled:
$$\frac{DK}{Dt} = \frac{\partial}{\partial x_j} \left(\frac{\nu_e}{G_k} \frac{\partial K}{\partial x_j} \right) + \nu_e \left(\frac{\partial^2 U_i}{\partial x_j^2} + \frac{\partial^2 U_j}{\partial x_i^2} \right) \frac{\partial U_i}{\partial x_j} - \epsilon$$

recall $\epsilon \sim \frac{u'^3}{l} \rightarrow \text{let } \epsilon = \underline{\text{const.}} \cdot \frac{u'^3}{l}$

Also let $u' \sim \sqrt{K}$; $l = \underline{\text{const.}} \cdot l_m$ ← mixing length

Let
$$\epsilon = C_D \frac{K^{3/2}}{l_m}$$

$C_D = \text{Dissipation Coefficient}$

See Eq (7) on Handout → our "one eq." for one-eg turb. model

Summary Unknowns: U_i, P, K, l_m (6)

4 primary transport eqs for U_i, P } (5)

1 extra transport eq for K

6th eq is not a transport eq., but must come from experiment \rightarrow typ. algebraic eq. for l_m

Note: $\nu_e = C_p \sqrt{K} l_m$ + constants C_p, C_0, G_k
also determined empirically

Does it work?

• We have added some "history" or "memory" effects for the turbulence since K is now a transport eq.
"better" than zero-eq. models

• But still not an ideal model since we need l_m from experiments

one-eq. models are not problem independent

[NOT UNIVERSAL]

5. Closure for Two Eq. Turbulence Models

a. Intro \rightarrow Any model lower than 2-eq. is "incomplete"

Why?

• Turbulence needs a minimum of two scales
• length scale
• velocity scale

\rightarrow zero-eq. models \rightarrow obtain both scales empirically \therefore locally

\rightarrow one-eq. " \rightarrow obtain K by a transport eq.

But $l_m =$ length scale \therefore still obtained empirically
 \therefore locally

The lowest level "complete" turbulence model is a two-eq. model"

add two transport eqs for the turbulence

$K-l$
 K -entropy ($\overline{w_i w_i}$)

K-ε model (most popular & widely used turbulence model)

↓

★ Still an eddy viscosity model

But → we don't need to supply a mixing length

★ Not a mixing length model

$$\nu_e = \text{const} \cdot l_m u'$$

→ But we will solve & model both l_m & u' in terms of K & ϵ to close the problem

Let $u' = \sqrt{K}$

$$\epsilon \sim \frac{u'^3}{l} \sim \frac{K^{3/2}}{l} \Rightarrow \text{Let } l_m = \text{const} \cdot l$$

$$l = \frac{K^{3/2}}{\epsilon}$$

$$l_m = \text{const} \frac{K^{3/2}}{\epsilon}$$

$$\nu_e = \text{const} \cdot \text{const} \frac{K^{3/2}}{\epsilon} K^{1/2}$$

$\equiv C_m$

$$\nu_e = C_m \frac{K^2}{\epsilon}$$

Notice — no more mixing length!

[Some people call this C_2]

K-ε model is still an eddy-viscosity model, but not a mixing-length model.

We already have a modeled transport eq. for K

We need a modeled transport eq. for ϵ

b. Exact Transport Eq. for ϵ if possible

(see Wilcox's book)

Rewrite ϵ eq. as

$$\frac{D\epsilon}{Dt} = \underbrace{\text{Diffusion or Transport of } \epsilon}_{\text{Diffusion or Transport of } \epsilon} + \underbrace{\text{Production of } \epsilon}_{\text{Production of } \epsilon} - \underbrace{\text{Dissipation of } \epsilon}_{\text{Dissipation of } \epsilon}$$

Total rate of change of ϵ

Model the entire RHS!

Keep LHS

C. Modeled Transport Eq. for ϵ

Model the ϵ eq. after the K eq. \rightarrow make it of the same form

High Reynolds # form of K transport eq.

$$\star \quad \frac{DK}{Dt} = \frac{\partial}{\partial x_j} \left(\frac{\nu_e}{\sigma_K} \frac{\partial K}{\partial x_j} \right) + \nu_e \left(\frac{\partial U_i}{\partial x_j} + \frac{\partial U_j}{\partial x_i} \right) \frac{\partial U_i}{\partial x_j} - \epsilon \quad (1)$$

High Reynolds # form of ϵ transport Eq.

[use the shovel heavily here!]

$$\star \quad \frac{D\epsilon}{Dt} = \frac{\partial}{\partial x_j} \left(\frac{\nu_e}{\sigma_\epsilon} \frac{\partial \epsilon}{\partial x_j} \right) + \frac{C_{\epsilon_1} \nu_e \epsilon}{K} \left(\frac{\partial U_i}{\partial x_j} + \frac{\partial U_j}{\partial x_i} \right) \frac{\partial U_i}{\partial x_j} - C_{\epsilon_2} \frac{\epsilon^2}{K}$$

Diffusion or transport of ϵ
Production of ϵ
Dissipation of ϵ

(gradient diffusion model)

5 constants in total \rightarrow Get these from experiments (decay of turbulence downstream of a screen) (BL's) (jets & shear layers)

$$\sigma_K = 1.0, \quad \sigma_\epsilon = 1.3, \quad C_{\mu} = 0.09, \quad C_{\epsilon_1} = 1.44, \quad C_{\epsilon_2} = 1.92$$

STANFORD
k- ϵ model

[Note: Some authors call it C_{ϵ_2} instead of C_{μ}]