

Today, we will:

- Continue to work through the example problem – fully developed turbulent channel flow
- Discuss the 3-layer model for wall-bounded flows – the law of the wall

Recall, x-momentum reduced to
$$0 = -\frac{\partial P}{\partial x} + \frac{d}{dy} \left[\mu \frac{dU}{dy} - \rho \overline{uv} \right] \quad (1)$$

and y-momentum reduced to
$$P = P_w(x) - \rho \overline{v^2}(y) \quad (2)$$

Plug (2) into (1): $\frac{\partial}{\partial x} (\text{fnc. of } y) = 0$

$$0 = -\frac{dP_w}{dx} + \frac{d}{dy} \left[\mu \frac{dU}{dy} - \rho \overline{uv} \right]$$

$$\frac{dP_w}{dx} = \frac{d}{dy} \left[\mu \frac{dU}{dy} - \rho \overline{uv} \right] \quad (4)$$

fnc. of x only = fnc. of y only **MUST = CONSTANT**

$$\frac{dP_w}{dx} = \text{constant}$$

P_w varies linearly with x

[same as in laminar flow]

$$\frac{d}{dy} \left[\mu \frac{dU}{dy} - \rho \overline{uv} \right] = \text{constant} = \frac{dP_w}{dx} \text{ or } \left(\frac{\partial P}{\partial x} \right) \text{ since } P = P_w - \rho \overline{v^2}$$

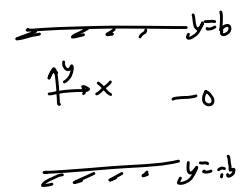
NOT A FNC. OF x

Integrate:

$$\mu \frac{dU}{dy} - \rho \overline{uv} = y \frac{\partial P}{\partial x} + C_1$$

Define $\overline{\tau} = \text{mean total stress} \equiv \mu \frac{dU}{dy} - \rho \overline{uv} = \text{fnc. of } y \text{ only (fully developed)}$

$$\overline{\tau} = y \frac{\partial P}{\partial x} + C_1 \quad (5)$$

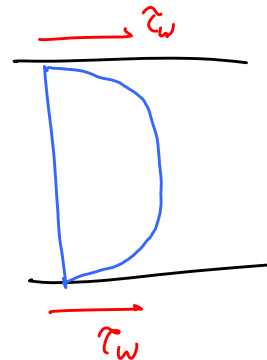


To find C_1 , apply BCs \rightarrow @ walls, $U=0, \overline{uv}=0, P=P_w$

@ $y = -b$ $\mu \left(\frac{dU}{dy} \right)_{y=-b} = \text{constant}$

Call this τ_w [Kundu calls it τ_0]

τ_w lower wall = positive



(5) becomes $\tau_w = -b \frac{\partial P}{\partial x} + C_1$ (6)

@ $y = b$, $\bar{u}v = 0$ $\mu \left(\frac{dU}{dy} \right)_{y=b} = \text{const}$, call this $-\tau_w$

(5) becomes $-\tau_w = b \frac{\partial P}{\partial x} + C_1$ (7)

Solve (6) & (7) simultaneously for unknown τ_w & C_1

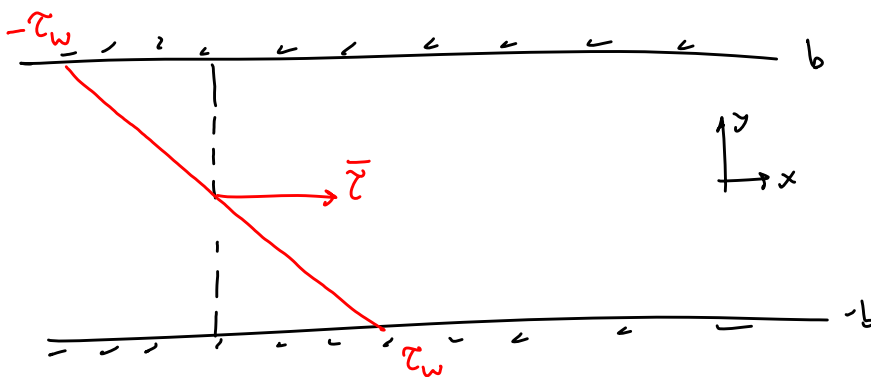
$C_1 = 0$! $\tau_w = -b \frac{\partial P}{\partial x}$ ★

So, (5) becomes $\bar{\tau} = \mu \frac{dU}{dy} - \rho \bar{u}v = y \frac{\partial P}{\partial x}$ (8a)

or, in terms of τ_w

$\bar{\tau} = \underbrace{\mu \frac{dU}{dy}}_{\text{laminar}} - \underbrace{\rho \bar{u}v}_{\text{turb}} = -\tau_w \frac{y}{b}$ (8b)

$\bar{\tau}$ varies linearly across the channel!



This is identical to the laminar channel flow result

$$\bar{\tau} = \underbrace{\mu \frac{dU}{dy}}_{\text{laminar shear stress}} - \underbrace{\rho \overline{uv}}_{\text{turbulent shear stress}}$$

Both lam & turb. shear stresses are nonlinear in y , but their sum ends up being linear in y

We can integrate again

$$(8a) \quad \div \mu \text{ i. rearrange} \quad \frac{dU}{dy} = \frac{1}{\nu} \overline{uv} + \frac{1}{\mu} \left(\frac{2P}{2x} \right) y$$

$\left[\nu = \frac{\mu}{\rho} \right]$
 \downarrow
const w.r.t. y

Int. from $y=-b$ to $y=y$

$$U(y) - \underbrace{U(-b)}_0 = \frac{1}{\nu} \int_{y=-b}^y \overline{uv} dy + \frac{1}{2\mu} \frac{2P}{2x} (y^2 - b^2)$$

$$U(y) = \frac{1}{\nu} \int_{y=-b}^y \overline{uv} dy + \frac{1}{2\mu} \frac{dP}{dx} (y^2 - b^2) \quad (9)$$

turbulent contribution

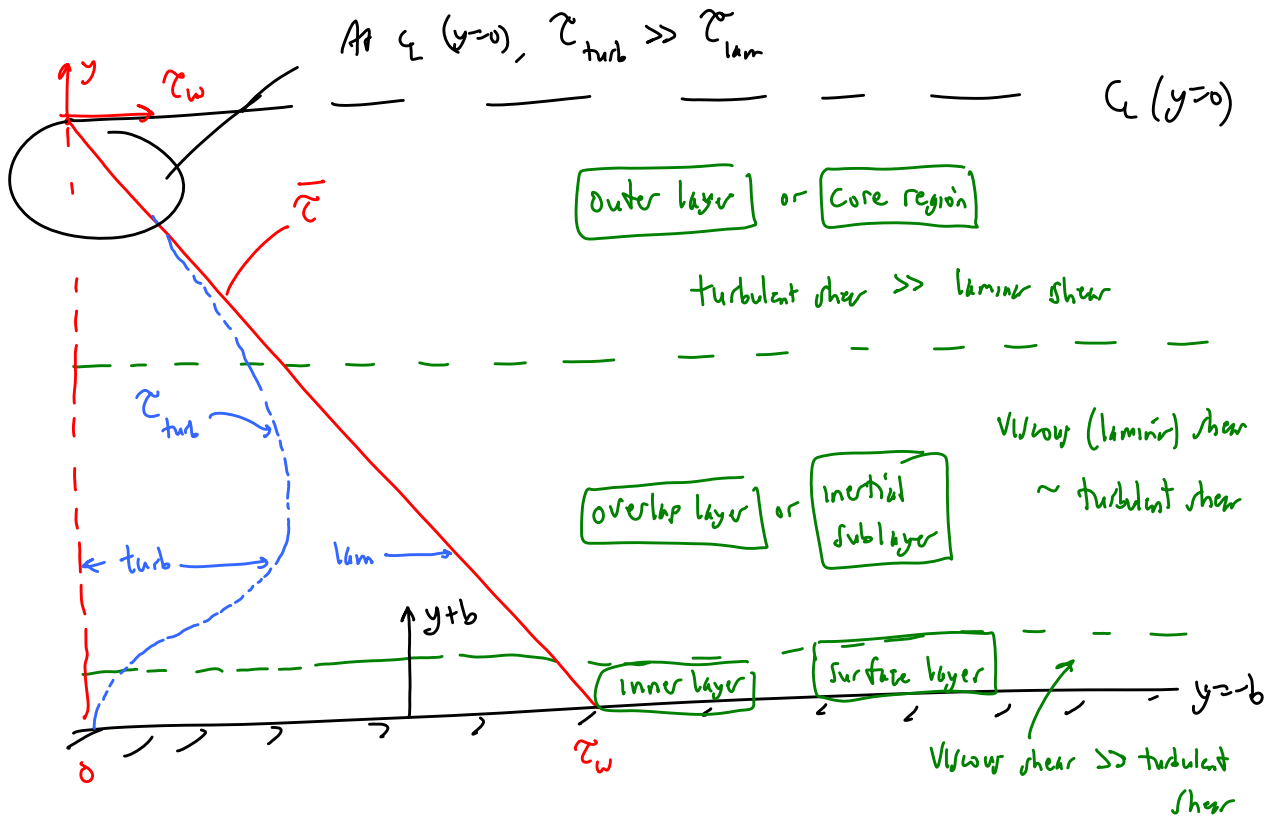
parabolic laminar-type contribution

This is as far as we can go analytically \rightarrow need to model \overline{uv}

Can solve for $U(y)$ if you model \overline{uv} with a turbulence model

b. Approximate Analysis using the Layered Approach

Split the lower half of the channel into 3 layers



At the wall, all of \bar{c} is laminar ($\overline{uv} = 0$)

Inner layer: expect $U = U(\mu, \rho, \tau_w, (y+b))$ (distance from lower wall)

[note: the flow in the inner layer, very close to the wall does not "know" or "care" about U_∞ ($U @ y=b$)]

Dimensional Analysis:

$$\left\{ \begin{array}{l} \Pi_1 = \frac{U}{\sqrt{\tau_w/\rho}} \\ \Pi_2 = \frac{(y+b)\sqrt{\tau_w/\rho}}{\mu} \end{array} \right.$$

Define Friction Velocity = $u^* \equiv \sqrt{\frac{\tau_w}{\rho}}$

a kind of Reynolds #

Notation:

| | | | |
|--------|---------|-------|-------|
| T & L | i, kunk | we | u^* |
| White | | u_w | v^* |
| Wilcox | | " | u_z |

$$\Pi_2 = \frac{(y+b) u^*}{\nu}$$

Define "Inner coordinates"
"Inner variables"

Let $\pi_1 = \frac{U}{u^*} = u^+ =$ inner velocity variable

Let $\pi_2 = \frac{(y+b)u^*}{\nu} = y^+ =$ inner coordinate
 or wall coordinate

Dim. anal. $\pi_1 = \text{func}(\pi_2)$ or vice-versa.

★ $u^+ = f(y^+)$ in the inner layer

★ "LAW OF THE WALL"

→ "universal" for any turbulent flow near a smooth solid wall

Eq (8b), recall, $\mu \frac{dU}{dy} - \rho \overline{uv} = -\tau_w \frac{y}{b}$ (8b)

In terms of inner variables:

we get $\frac{du^+}{dy^+} - \frac{\overline{uv}}{u^{*2}} = 1 - \frac{y^+}{R^*}$ (11)

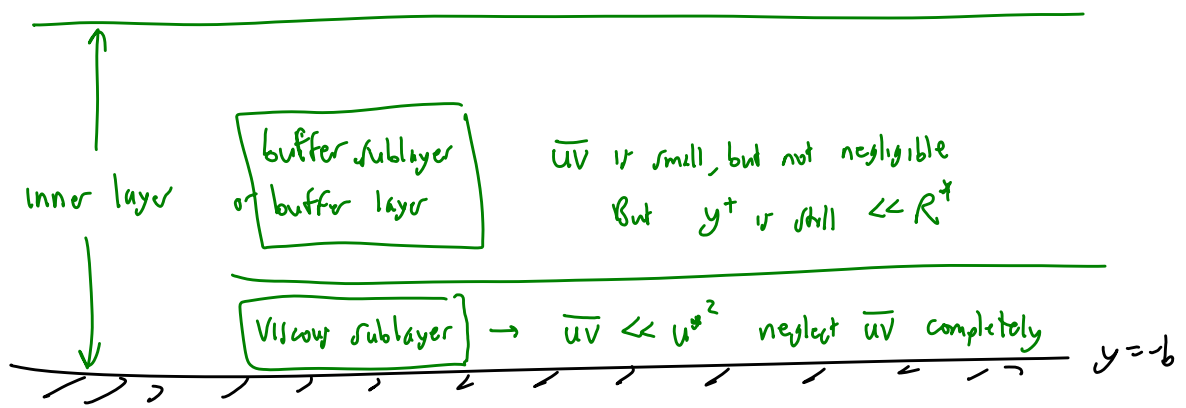
where $R^* = \frac{u^* b}{\nu} = y^+ @ \text{ centerline of the channel}$

In the inner layer, $y^+ \ll R^*$

In inner layer, (11) becomes

$\frac{du^+}{dy^+} - \frac{\overline{uv}}{u^{*2}} \approx 1$ (11 i)

Let's split the inner layer itself into two layers:



In viscous sublayer, (11 i) becomes $\frac{du^+}{dy^+} - \frac{\bar{u}\bar{v}}{u_*'^2} \approx 1 \Rightarrow \underline{du^+ = dy^+}$

≈ 0

integrate: $u^+ = y^+ + \text{const}$
 \hookrightarrow @ $y = -b$ (at wall), $y^+ = 0$, $u^+ = 0$, $\text{const} = 0$

★ $u^+ = y^+$ in the viscous sublayer of the inner layer

in physical variables, U varies linearly with y

also called the linear sublayer or laminar sublayer

Experimentally, the viscous sublayer extends to approx. 5 wall units from the wall

$u^+ \approx y^+$ for $0 \leq y^+ \leq 5$ ★